

Verification Report for

: TEIL Biomass Grid Supply Power Project, Khatauli, Uttar **Project**

Pradesh

UCR Project ID : 261

Name of Verifier	SQAC Certification Pvt. Ltd.
Date of Issue	August 29, 2023
Project Proponent	Triveni Engineering and Industries Ltd. (TEIL)
UCR Project Aggregator	Carbon Equalizers, Katni
Work carried by	Mr. Santosh Nair
Work reviewed by	Mr. Praful Shinganapurkar

Summary:

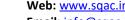
SQAC Certification Pvt. Ltd. has performed verification of the "TEIL Biomass Grid Supply Power Project, Khatauli, Uttar Pradesh, India". The purpose of the project activity is to generate electricity using renewable biomass and thereby reduce GHG emissions by displacing fossil fuel dominated grid based electricity with biomass based renewable electricity.

Verification for the period: 01/01/2013 to 31/12/2022

The GHG emission reductions were calculated on the basis of UCR Standard for Baseline Grid Emission Factor, CDM UNFCCC Methodology, ACM0006: Grid connected renewable electricity generation (Ver.16.0). The verification was done remotely by way of video calls / verification, phone calls and submission of documents for verification through emails.

SQAC is able to certify that the emission reductions from TEIL Biomass Grid Supply Power Project, Khatauli, Uttar Pradesh, India, (UCR ID -261) for the period 01/01/2013 to 31/12/2022 amounts to 8,62,201 tCO₂ (8,62,201 CoUs)

Accredited by 5 Jupiter House, Callera Park, Aldermaston, Reading Berkshire RG7 8NN, United Kingdom (UK). India Office: Off. No. 4, Fifth Floor, Buildmore Business Park, New Canca Bypass Road, Khorlim, Mapusa, Goa – 403 507



Email: <u>info@sqac.in</u> Tel: 7219716786 / 87



Detailed Verification Report:

Purpose:

The project activity involves the renewable biomass (bagasse) based electricity generation within the Triveni Engineering & Industries Ltd (TEIL) plant located at City: Khatauli, State: Uttar Pradesh. This UCR project activity involves the installation of two 23 MW turbo generators along with two high pressure (86 kg/cm²) 120 TPH capacity boilers commissioned in 19/10/2005 and 17/12/2006. The total installed capacity is hence 46 MW.

The power generated from the turbines is utilised for captive consumption and the surplus power is exported to the grid. Power is generated both in the sugar season and off-season at 11 kV and stepped-up on-site to 132 kV before being transmitted to the nearby UPPCL sub-station located at Khatauli.

Office of Executive Engineer
Electricity Distribution Division
PASCHIMANCHAL VIDYUT VITRAN NIGAM Ltd.
Muzaffarnagar (Uttar Pradesh)

Certificate of commissioning

This is to certify that M/s Triveni Engineering & Industries Ltd. Unit-Khatauli, Distt. Muzaffarnagar (U.P.) is having valid Power Purchase Agreement with PVVNL. The commissioning details of their bagasse based co-generation units as per PPA & our records are as follows:-

Unit Numbe	Unit Number, Capacity and Date of Commissioning Details									
Unit No.	Capacity	Date of Commissioning								
1	23.0 MW	19/10/05								
2	23.0 MW	17/12/06								

UPPCL Nodal Officer Executive Engineer (Distribution)

Location:Muzaffarnagar विकृत वितरण वण्ड

नुजनफरनगर



The UCR project activity is the construction and operation of a power plant/unit that uses renewable energy sources and supplies renewable electricity to the grid. The UCR project activity is thus the displacement of electricity that would be provided to the grid by more-GHG-intensive means and provides long-term benefits to the mitigation of climate change. The UCR project activity qualifies under the environmental additional positive list of pre-approved project types under the UCR carbon incentive model for issuance of voluntary carbon credits.







Location of project activity:

Country : India

Village : Sheikhpura, City : Khatauli,

District : Muzaffarnagar State : Uttar Pradesh (UP)

Pin : 251201 Latitude : 29° 16′ N Longitude : 77° 42′ E





Scope:

The scope covers verification of emission reductions from the project - TEIL Biomass Grid Supply Power Project, Khatauli, Uttar Pradesh, India, (UCR ID -261).

Criteria:

Verification criteria is as per the requirements of UCR Standard.



Description of project:

The UCR project activity is a grid-connected biomass (bagasse-based) cogeneration power plant with a high-pressure steam-turbine configuration. The high-pressure boilers are fired by bagasse, a biomass by-product from the sugar manufacturing process, to generate steam which in turn is fed to the steam turbine to generate power. The overall business is integrated with alcohol distillation and power generation. The power co-generation units generate biomass-based power for captive consumption of the sugar plant and the sale of surplus power to the state grid. The project plant exports power to the Uttar Pradesh Power Corporation Limited (UPPCL), in absence of the project activity, UPPCL would have withdrawn electricity from northern regional grid.

The project activity has commissioned two (2) boilers with nominal capacity of 120 tons per hour (TPH) and outlet steam configuration of maximum capacity 87 kg/cm², 515°C and two turbo generators with rating of 23 MW each (total 46 MW). The cogeneration cycle for the plant is designed as an energy efficient regenerative cycle.

The power is generated at 11 kV level. The internal consumption requirements for auxiliaries and equipment of the sugar plant and the cogeneration plant are met by stepping down voltage level to 415V. The exportable power is stepped up to 132 kV and paralleled with the UPPCL grid at the substation in Khatauli.

	Phase-1	Phase-2
Turbine		
Capacity (MW)	23	23
Steam Pressure	84 kg/cm² (G)	84 kg/cm ² (G)
Steam temp.	510 °C	510 °C
Year of Commissioning	2005	2006
Boiler		
Capacity (Tons/hr)	120	120
Year of Commissioning	2005	2006
Steam temp.	86 kg/cm² (G)	86 kg/cm² (G)
Steam pressure	515±5 °C	515±5 °C



INSTRUM	ENT DETAILS							
Steam Flow:								
Make	Rosemount.							
Sr. No	S 0226515							
Steam Pressure:								
Make	Rosemount							
Sr. No	S 0226501							
Steam Te	mperature:							
Make Rosemount								
Sr. No S-225016								

Level of Assurance:

The verification report is based on the information collected through interviews conducted over video calls / phone calls, supporting documents provided during the verification, Project Concept Note (PCN) / Monitoring Report (MR), submitted to SQAC. The verification opinion is assured provided the credibility of all the above.

Review of the following documentation was done by SQAC Verifier, Mr. Santosh Nair, who is experienced in such projects.

Documentation Verified:

- Project Concept Note (PCN)
- Monitoring Report (MR)
- JMR's
- Month wise Quantity of biomass residue combusted in the project plant.
- Commissioning Certificate
- Calibration Certificates
- Power Purchase Agreement
- Invoices



Sampling:

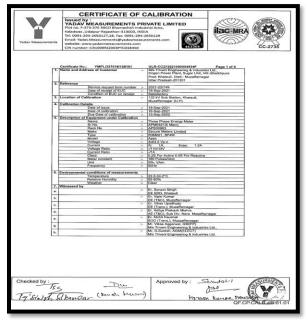
Not applicable

Person interviewed:

Mr. Ashish Awasthi
 Mr. Manish Saxena
 Triveni Engineering and Industries Ltd.
 Mr. Vipin Jindal
 Mr. Vikas
 Triveni Engineering and Industries Ltd.
 Triveni Engineering and Industries Ltd.



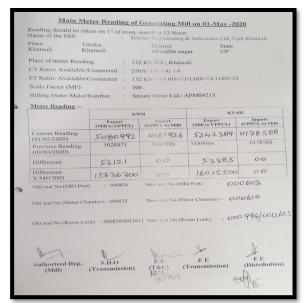


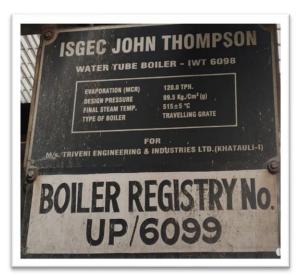






_	INVOICE OF POWER PURCHASE BY DISCOM/U	PPCL FROM C	DEFECTION
For the M	onth of		April-2020(01/04/2020 to 1/05/2020)
			COGEN/PPA/20-21/01 Dwtd- /05/2020
Monthly 9	Purchase Bill Ref. No.		11/6759
Date of su	abmission of bill to Nodal Officer		
Name of	Buyer		U.P. Power Corporation Limited 14, Ashok Marg. Shakti Bhawan Lucknow (UP)
Name of	Generating Plant		M/s TRIVENI ENGINEERING & IND. LTD., VIII-Sheikpura, Khatauli, Muzaffarnagar (UP) – 251 201
SI. No.	DESCRIPTION	TUNIT	
A A	Energy Supplied as per JMR	Kwh	15636300
8	M.F. for compensation of Transmission Losses		1.001532
C	Net energy after compensation of transmission loss (A*B)	Kwh	15660255
D	Energy for Banking	Kwh	2688000
E	Net Energy (C-D)	Kwh	
F	Rate of Energy	Rs./Kwh	2.9-
G	Net Amount For Payment (E*F)	Rs.	3813843
_	BANKING ACCOUNT	TUNIT	
_		Kwh	48538
a	Opening Balance Energy Banked during month	Kwh	268800
b	Less 12% Banking Charges (b*0.12)	Kwh	32256
C	Balance (a+b-c)	Kwh	285082
d	Less Energy Consumed during the Month	Kwh	
0	Balance B/F (d-e)	Kwh	285075
Authoris	ad Signatory	Ele	Executive Engineer setticity Distribution Division







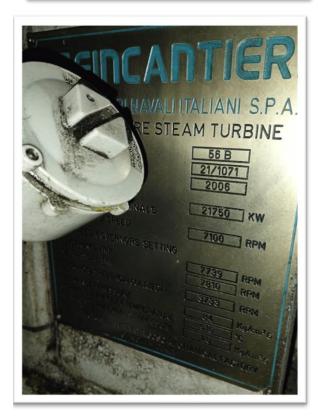


8	DILER LOG BOOK		C	o-Gener	ation Un				Date : e	olse	3/2	023	
S. No	Service Parameters	Unit	15:00	18:00	17:00 T	B-S	hift 19:0	0 20	100	21:00	1 22	00	
3	Main Steam Flow	TPH	116-8	116	115.7	116-2	116	1 "	6	116.4	10	6	
2	Main Steam Pressure	Kg/Cm ³	83.5	84	85.6	-	88			85-	2		A.
3	Main Steam Temp.	*0	5708	502	500	50b	55 1	. =	06	con	10	05	4
4	Fuel Feeding	76	tro	tro	23.6	37	25	= 1	46	34	1	+0	4
5	Feed Water Flow	M'/H	109	106	106	406	10	1 1	09	98	8 1	06	4
6	Feed Water pressure	Kg/Cm*	tol	101	101-2	101	101		10	101	-	101	Щ
7	Spray Water Flow	TPH	9.2	5-14	8.5	7.5	9	-1	8.2	9		9.5	
8	Drum level	%	51.b	512	500	201	04	8	45 Y	532	-6	Sic	
0	Drum Pressurs	Kg/Cm ¹	88.6	88-7	90.3	90	8	9 :	39	80		88	
10	Primary B/H Outlet Temp.	*0	472	461	476	468	3 4	lb	468	7700	30	14-7	
11	Secondary S/H Inlet Temp.	*c	383	288	384	38	1 3	85	385	10000	83	38	
12	Feed Water Temp. at Eco M.	*c	148	148-8	148.8	140	1 (1	100	14.8	14		114	
13	Feed Water Temp. at Eco. CVL	*c	268	268	270	200	3 2	TO	265	3 5	89	2	
14	F.D. Fans disch. Pr. APH Inlet	MMWC	97	98	102	103	3 0	16	100		05	10	
15	F.D. Fans disch. Pr. APH Outlet	MMWC	50	46	42	47		(3	143		+5		
16	F.D. Air Temp at APH Inlet	*c	26.3	2.6.5	25.8	3 24	.5 9	3.6	22.	1 2	1-7	2	
17	F.D. Air Temp at APH Outlet	*c	120-7	120	120	110		17	115	1	118	1	11:
10	F.D. Air Flow	TPH	192	103	193	9 19	14 1	96	19-) 1	98	1	10
19	S.A. Fans Discharge air Pr.	MMWC	450	638	4.55	45	50-1	442	43	1 1	+50	1	10
20	S.A. Fan Air Flow	TPH	79.7	79.	6 80	180	-81	20.0	81.	5	80.	8 .	8
21	S.A. Fan Discharge air Temp.	°C	138	138	137	12	57	136	13	4	134	-8	15
22	O. in Flue Gas	56	1.2	3.5	3-2	3 3.	3	5-3	4.	2	3.0	5	14
23	Furnace Pressure	MMWC	18.7	9.2			100	12.	5	-4	7-	2	**
24	Furnace Temp.	°C	762	738	3 73	A 100 Person		715	-	31	14	2-	
25	Deserator Level	%	60-1	60	60	6	0	60 -	2 5	7.5	60		6
26	Deparator Pressure	Kg/Cm*	-672	-65	5 .66	6 -	666	-66	8 -1	230	-6	62	1
27	Desorator Temp.	'c	115.4	1	4 115	3 11	5.8	115-	5 11	5	-	2.5	1
28	Deserator Steam Flow	TPH	6.7	6.1	6 6.	5 6	0.7	500	7 6	.1	7		A)
29	Condensate Flow	трн	137	13	-	C 100	37	13	8 1	38	15	38	4
000	SA-1 Speed	96	82	82			32	83	2 5	32		32	4
223	SA-1 Speed SA-2 Speed	76	82	89			82-	8	2 5	32	1 8	32	3



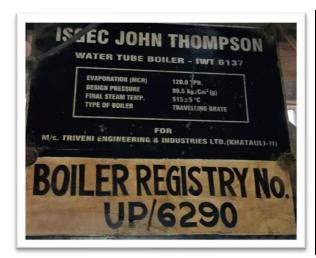
U	RBO GENERATOR-I LOG BOO	OK	enerati							Di	ate [2910	8120	25
	Service Parameters	Unit	23:00	24	1:00	01:00	02	C-Shi	3:00	04:0	10	05:00	06	00
	Turbine Load	MW	20.54	90	0.0	9.00	200	20 11	18.0	193	-77	9,72	2.0	10
	Turbine Speed	RPM	5525			325	22		426	100		Sal	55	
	Inter Steam Pr.	Kg/Cm ²	044	0		2003			000	70	62.1	525	00	1.0
	Inter Steam Temp.	°C	202	5		504	2	00	503	22	9	202	6	92
	Inter Steam Flow	TPH	113-8	1	3.2	112.0	11		111.2		1.0	111:		3.9
	Casing Expension FE	mm	11-022			DETS!			11.19		1000	11.6	DE 11	- 60
	Axial Displacement	mm	-0.53		184	0.04		39				-0.5	4	105
	Rotor Differential Expension	*C	0.09		1000000		100				:220		Tan-C	
	Casing Metal Temp.	Kg/Cm³	112						441			44		44
	Wheel Case Pr.	Kg/Cm ²	49.3			490			13.					19
	9/13 ata Extraction Steam Pr.	*C	9.28		7.52	9.6	10	1-61	9.0	24 100	1.42		4	101
	9/13 ata Extraction Steam Temp.	TPH	106		067	187		901	9.1		0.0	118	77	9.1
	9/13 ata Extraction Steam Flow	Kg/Cm²	8.91		9.29	9.0		9.91			J.9.		123	1-0
	3 ata Extraction Steam Pr.	*C	1.30,		433	1-4	-	. 375	19		49		48	14
	3 ata Extraction Steam Temp.	TPH	100		477	140.	100	48			31.8		2,0	03
	3 ata Extraction Steam Flow	Kg/Cm²	84		93110			33.74		-	9.11		15	9.
	87/13 ata Aux. Steam Pressure	*C	8:73		88.8	8-3		795	20		290		93	20
	87/13 ata Aux, Steam Temp.	Kg/Cm²	39		390					took-	0-0		1034	0.
	Sealing Steam Pr.	*C	0.04	0 1	09/33	399	2	2000	387				36/20	
	Sealing Steam Temp.										60		0.90	0
	Exhaust Steam Pr./Vaccum	Kg/Cm²	CONTRACTOR OF THE PARTY OF THE	100	0.89					-	47	200	47.8	
	Exhaust Steam Temp.	°C			47.5			47.3		1.3	20	~	21.0	1
В	Exhaust Steam Flow	TPH	23	201	20.5			74	-	1.9	79	-0.	72	1
	HP Valve Demand	%	73		75	0/		-	1000	10	01		ite	100
	LP Valve Demand	%	0(2		0120	-	-	012	1000	9	13		133	1
	Control Oil Pressure	Kg/Cm	1-1-2-		139	13		135		4-2	30		26	1123
	Control Oil Temp.	°C	360	5	36.5			30.0		107	22		5/4	
Ī	Turbine Thrust Brg. Temp. (Non-Active)	,c			5/57					-/15	66		66/4	-
Ī	Turbine Thrust Brg. Temp. (Active)	°C	66/	22	6712	1 66	22	66/5	200	1000				-
t	Turbine Front Brg. Temp.	'C	63		63	6	1000	63		33		3	C.3	-
ŀ	Turbine Rear Brg. Temp.	'C	7	6	76	7	7_	-10		77		77	79	
h	Pinion F/Brg. Temp.	*C	1 -7	0	70	7	9	3.5	1	70		70	73	MINE IN
H	Pinion R/Brg. Temp.	°C	8	4	04	8	14	8	1	03	1	83	8	
	Gear Wheel F/Brg. Temp.	°C		9	69	6	9	6	9	69	1	92	1000000	9
L	Gear Wheel R/Brg. Temp.	°C		10	0		0	6	0	80	1	BO	0	0
L	Gen. F/Brg. Temp.	°C	- Inches	9	-		-9	-		(3)	1	92	5	0
L	Gen. R/Brg. Temp.	'c		-3	63		33	6	3	63		63		3
Ŀ	- Carlotte Control Control	1127	0.0		22/3		127	0		2/35		127	22/	37
L	Turbine Front Shaft Vibration	Micron			26/1		41			6/11		7/16	27/	16
L	Turbine Rear Shaft Vibration	Micron				10000				212	0	121	12/	4
L	Pinoin Front Shaft Vibration	Micror				-	121			6/8	-	10	61	0
I	Pinion Rear Shaft Vibration	Micror	one or the same		6/8	-	10		9	121	-	411	121	100400
	Gear Front Shaft Vibration	Micror			12/1		10	12	- District	911		113	100000	113
	Gear Rear Shaft Vibration	Micror	18 41	13	911		113		12		3	50/01		145
	Gen. Front Shaft Vibration	Micro	ns 6/	40	60/	40 61	100	120	148	6010	2011	6916		16

							B-Sh	19:00	20:00	21:00	22:10
_			Unit	TO RESIDEN	16:00	17:00	18:00		96	96	96
S. No	Service	Parameters	Unit	15:00		96	96	96	97	94	97
32	FD-1 Speed		%	96	96	97	94	97	99	99	94
33	FD-2 Speed		%	97	97	an	99	99	99	99	95
34	ID-1 Speed	4241 10 1	%	99	99	99	99	94		2	
35	ID-2 Speed	Sign May	%	99	99		11_	8	4	-44	10
36	Flue Gas Pre	ssure at Eco VL	MMWC	8	10	14	_48	-46	-48	1	-41
37	Flue Gas Pre	ssure at Eco O/L	MMWC	-48	-44	100000	-98	-96	-018	400	100
38	Flue Gas pre	ssure at APH I/L	MMWC	-96	-98	-92	148	-144	120	-125	10
39	Flue Gas Pre	ssure at APH O/L	MMWC	148	-148	-144	THE	-144	150	1720	- 128
		essure at ESP I/L	MMWC	148	446	144		-200	-208	-211	210
		essure at ESP O/L	MMWC	-118	-210	-212	-204	-	444	144	R 449:
	Flue Gas Ter		°C	449.9	449.2	445	444	488		-	232
		np. at Eco. O/L	*c	236	936	236	236	2350	235	Total Street	
			*c	227	227	937.2	227	1 228	227	-	STATE OF THE PARTY OF
	Flue Gas Ter		¹c	1338	134	133.6	133.	1 152.8	152	0 131	0 130
		mp. at ESP I/L		1	100 m 1 m 1 m 1 m 1 m 1 m 1 m 1 m 1 m 1	129.0	128.6	AL FIELD FOR	1 127	D 123	12 126
46	Flue Gas Te	mp at ESP O/L	"C	129.6	129-2		94	91	85	2 8	24 8
47	Feed Water	Tank Levie	*,	92	1	92	1	2.8	2 6,5	p 6	.48 6
48	Instrument A	Air Pressure	Kg/Cm ¹	6.48	6.51	6.50	6.5	0	- 6r-	0 0	-
Fe	ed Pump-1	4				Laurin	- 10	must be	eted	duri	~a
Fe	ed Pump-2	allow-	arks	2 \$	004 P	100014		mand.	9)
Fe	ed Pump-3	_		the	ine	4	_				
TF	R Pump-1	×					1.			0 1	uston.
TF	R Pump-2	N <	X	B. F. 1	0.30	yea co	nucedi	04 6	LOXE	cono	Mayor.
IA	C-1	A	A A	1 4-	road s	60	1 5	Trolling			
IA	C-2	4 1	X	211	-	00	2001	00111	73		
IA	C-3	L							2		
Di	PC-1	L									
DI	PC-2	7									
	CBO% Crack Mana Vanna										
100	o. of IBD	Contract Contract	S Engr.	y can	mon		Mary				
	V. W. IDU	100	J Liigi.				110				
	200	COLUMN TOWN					The same of the	We will be	THE PARTY NAMED IN		









			-	C	3/3							
		Irive	ni En	gineer Genera	ing 8	Ind	lustr	ies L	tcl.			
10	ILER LOG BOOK	-		-Genera	tion Un				Date:	59.0	94.24	
5.	Bervice Parameters	Unit	15:00	10:00 1	17:00 I	18:00	Shire 19:	on I an	00 1	21:00	22.00	
	Adale: Unedert Flerw	TFIFE	114.0	1134.0	1754-1	1104			And the same	(151-3	114.0	
	Main Glean Pressure	Kg/Dm*	24.6	10.14+10	9.64	M. L.	16.70		4.4.4	R = 1.	SLEAM	
	Mars Oseam Temp.	*(0)	202	X10	500	201.0	No. No.		1000	201 NO	1514	
4	Fuel Feeding	14	4 %	524	0.20	× 1.		162 1	U.S.	-	56	
	Feed Water Flow	845/64	110	106	104	100	11 0	0 1		1100	100	8
0	Food Water preseure	Kg/Cm ^e	1.04.6	100014	NUMBER	X100.	W 10	3 - h V	na · to	1024		Delta del
	Spray Water Flow	TPH	6-1	2-4	4.14	10.0	. 8	1 50	p to	0.0	7.8	
0.	Corum terced	16	** en	100.00	50	132.0	1 1 36	0.0	50	20	20	
9	Drum Pressure	Ky/Cm ³	St. R. S	29.1	29.4	2.3	N A		E9-2-	29-5		
10	Primary Edit Outlet Temp.	*(3	M 6.8	N2 A	444	1904	1 4	74 L	MELY	1.43		
9.9	Secondary 5/H friet Temp	- 100	2.3. 3	290	2014	29			200	200		
12	Feed Water Temp. at Eco VI.	- fc	114-8	114-8	5554.20	115	and the second		112	112	14.5	
10	Feed Weter Temp. at Eco. Ort.	*0	aunib	241.5	241-1			21115	341-1			
14	F.D. Fans disch. Pr. APH svet	MMWC	1.62	164	100	16	-	0.2	100	100	-	
1.0	F.D. Fane duch. Pr. APH Outle	MMWC	10.9	13.2	124	10		12 0	100	100		2.24
10	F.D. Air Temp at APH Inlet	*63	200	0.41	24-1	20	36	72-7-12	201		STATE OF THE PARTY.	50.4
17	F.D. Air Temp at AIPH Outliet	*0	1552	1,3500	IPED.			1sterp	12350		-	69.4
3.0	F.D. Air Flow	TEH	186	165	160		250	150	1 24			90
7.0	S.A. Pans Discharge air Pr.	MANAGE		MED	464	-	68	420	40	100	A CONTRACTOR OF THE PARTY OF TH	
220	S.A. Fan Air Flow	Trees	69.8	64.8	69	and other	46	69.4	63	Access 1 married	59.4	1000
21	S.A. Fan Discharge sir Temp.	*c	1 66	1.6.6	161	10000	56	104	10	-		21.1
	O, in Flue Gas	- 96	3-14	Lit	. 4.	6	1-4	4.4	-	- 1	11-6	
23		MMVVC	3 %	C.	11		10	8	6	1	101	4115
24	A CONTRACTOR OF THE PARTY OF TH	*G	Ret	10 52	o +4.50	6	5610	204		-	124	
	A STATE OF THE PARTY OF THE PAR	100	D. C	0.0	2	0	60	60	-	0	60	60
	S Distribution Control	Калоп	. e. E. S!	9	4 0.8	4 .	125	65.0			25	0 - 5
	4 Read Part State Control	*c	115	115	111	-	110	HE	11	(5)	112	115
gii.		TPH	-	-	100	2.4	818	150	20	200	2-3	15.
Œ	Deserator Steam Flow	TPH		19.5	7.5	2.	12.4	121	1	2	121	13
150	D Condensate Flow		8.0	- April 100		0	80	8	63	20	. 20	100
3	O SA-1 Speed	76	-	-		80	20	8	0	20	200	
3	1 SA-2 Speed	16	81	2 36	-	4-		-				





BC	ILER LOG BOOK	-		-Genera	tion Un	it, Khat	auli		Date:	29.0	34.25	
B. Mon	Service Parameters	Unit	15:00 1	10:00 1	17:00	B-S	hift	0 1 20		11:00	22:00	
	Asin Steam Flow	TPH	114.0		154-1	1100-4			-	14-2	114-0	
	Main Steam Pressure	Karom*	231.60	8448	2004	× 1.	10.00	-	www.	ROL	25.5	
	Main Steam Temp.	*C	802	510	508	210	150		0.5	5110	572	
d	Fool Feeding	96	48	15M	50	×1.	1	10	182	54	56	
.6	Feed Water Flow	M264	110	106	Mar	108	11	0 1		110	10	8
0	Feed Water pressure	Kg/Cim²	1 back	104-4	NONE	140 × 8	10	A . L	4.6	1020		2000
	Spray Water Flow	TPH	8-1	2.4	2.4	4. 1	- 8	. 8 2	100	9-0	708	
8	Casam level	.76	50	2.0	50	42	×	0	00	20	20	
9	Drum Pressure	Kg/Cm ³	2.8	29.1	89.4	29.	8 A	3.6 7	9.2	29.5		-
10	Primary S/H Outlet Temp.	*0	M 6 8	14.40	444	44 2	- 4	4.0	424	1.45		
11	Secondary IS/H In/et Temp.	***	2. 2. X	390	294	291			90	50,		
12	Feed Water Temp. at Eco I/L.	, *c	114.5	114-8	11-4.5		11	2 1	12	112	111	_
10	Feed Weter Temp. at Eco. O.L.	*0	241.6	2.41.9	341-1	341.			24110	341		
14	F.D. Fans disch. Pr. APH Inlet	MMWC	1.62	164	100	180			100	163		24
10	F.D. Fans disch. Pr. APH Outle	NMWC	10.7	13.2	124	10	-		104	10	770000	10.0
10	F.O. Air Temp at APH felet	*C	320	35.1	3.11-1	2,25	2	351	2215		-	19.4
17	F.D. Air Terrip at APH Outlet	40	145	171.2	10000			10417	1011.4			90
18	F.D. Air Flow	трн	187	155	188	Conference (con-	-	18 P	1 89.	777		454
11	S.A. Fans Discharge sir Pr.	MMWC	PZP	420	464	Ne		120	45	0	-	40.6
20	S.A. Fan Air Flow	TPH	69.8	69.8	60	-	1.6	69.4	69.	-	9.4	
21	S.A. Fan Discharge air Temp.	10	166	106	161		-	184	10	-	- Charles	104
22	O, in Flue Gas	16	2.44	Line	. 4.	6 4	H	4.4	11-	1	4.6	
22	Furnace Pressure	MMVVC	9.	0	11	1	0	8	6		(0)	475
2	1	*C	g o t	200	o +40	0	210	204	179	Acres 1	124	
21		96	60	60	B	0 (50	80	6		-60	60
25	A PARTICIPATION OF THE PARTICI	Ka/Crr	. D. E. 3!	4 m.8'	8.0	MO	25	0.2	and the same of	-	2.5	0 - 8
2	A proposed and the control	*C	115	Contract of the last	111	5	115	115	111		112	115
II.	Contract Con	TPH	5	-	3/3	2.	202	150	8 2	20	2.3	15.
2	C Property and Comments of the	(milate)	1.00	122	115	2	12.1	121	1	20	121	13.
2	Street Control	TPH	80		-	0	80	80	3 9	20	. 20	8
3	O SA-1 Speed	96	81	-	-	80	20	18	0	20	21	

								0.5	Shift			
B. No.		Service P	'arameters	Unit	15:00	T 18:00	17:00	18:00	19:00	20:00	21:00	22:00
39	Lube	Oil Supply Pr	At OB Brg.	Kg/Cm ⁴	1.0	1.0	1.8	1-0	1.62	1.0	1.0	1:0
40	Lube	Oil Supply Pr	At Gen. F/Brg.	Kg/Cm*	1.5	1.5	1.5	1.5	1.5	1-5	1.2	1.5
41	Lube	Oil Supply Pr	At Gen. R/Brg.	Kg/Gm*	1.3	1-7-	1-9	1.7	1.7	1-7	1.3	1.7
42	Lube	Oil Return Ter	mp. Turbine F/Brg.	°C	15.54	54	54	54	54	54	54	2.5
43	Lube	Oil Return Ter	np. Turbine R/Brg.	*0	44	43	47	42	49	49	49	32
44	Lube	Oil Return Ter	mp. at G/Brg.	°C	50	59	59	2.5	55	24	59	2.4
45	Lube	Oil Return Ter	np. Gen F/Brg.	*C	52	.5-2	52	5.2	5.2	53	22	5.5
46	Lube	Oil Return Ter	np. Gen R/Brg.	*C	51	51	51	51	12	51	51	51
47	Oll Co	ioler Oil Inlet T	femp.	*C3	62.0	61.9	04.0	62.9	cers	62.7	62.59	66.8
415	Oil Co	oler Oil Outlet	Temp.	*C	Crass	100.5	40-3	No.1	Cost	1-012	6004	401
49	Oil Co	oler Oil Inlet F	Pr.	Kg/Cm*	9.5	9.5	9.5	2.5	9.4	2.5	9.5	95
50	Oil Co	oler Oil Outlet	Py.	Kg/Cm*	1.9	1.9	1.9	1.9	1.9	1.9	1.9	1.9
51 1	Oil Co	ofer Cooling V	Vater Inlet pr.	Kg/Cm*	400	410	400	400	400	60.00	Section	410
12	Oil Co	oler Cooling V	Vater Outlet pr.	Kg/Cm*	3.0	3-0	3+0	3.0	3.0	3.0	3.0	3.0
3 4	Oll Co	oler Cooling V	Vater Inlet Temp.	*C	29	2.0	.2.9	29	29	2.9	2.0	29
4 0	Oil Co	oler Cooling V	Vater outlet Temp.	*C	33	35	33	33	34	33	33	35
5 /	ACW	Discharge pr.		Kg/Cm*	5.3	5-5	5.3	5.3	2.2	53	B. C.	53
6 7	ACW I	Discharge Ten	ip.	*c	29.0	200	20.7	30.9	20.9	20.9	200	20.9
7 0	SVC 5	uction Pr	11-12-1	MMWC	-40	-40	-40	-40	-40	-40	-40	-40
8 0	SVC S	uction Temp		*c	310	310	310	310	310	310	310	310
0	en. C	ooling Water I	nlet Temp.	'c	20	29	29	29	29	29	2.9	29
G	ien. C	poling Water (Outlet Temp.	*c	31	31	31	31	31	31		31
G	en C	ooling Water I	nlet pr.	Kg/Cm²	4.4	THE REAL PROPERTY.					31	
G	en Co	ooling Water C	Outlet pr	Kg/Cm³	3.0	tests	4.4	April .	Cree	4.4	Serve	4.4
Di	ff. Pr.	Across Lube (Oil Filter	Kg/Cm³	THE RESIDENCE IN	3160	3.0	340	3.0	3:00	3.0	3.0
		Tank level		mm	21.0	0.11	045	0:11	0.17	0.11	0.11	0-15
		Tank Overflo		Yes/No	410	400	410	410	CILO	410	MID	410
OP		AOP-2	EOP I	JOP		CW-C	1	-	-	1	-	1
	-	ACF-2	EOF	JOP	1	CVV-C	AC	CW-D		BLOWER	GVC	BLOWE
	-				1 100		1		0	0	(1)
	arks		Noumer.								-	
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	mar.											
-	angr.											Shift I/



Applied methodologies and standardized baselines:

UCR Protocol Standard Baseline

SECTORAL SCOPE - 01 Energy industries (Renewable/Non-renewable sources)

TYPE I - Renewable Energy Projects (Large Scale)

UCR Positive List Environmental Additionality

SCALE - Large Scale

CATEGORY- ACM0006 Large-scale Consolidated Methodology Electricity and heat generation from biomass, Version 16.0

This methodology is applicable to project activities that operate biomass (co-) fired. power and-heat plants. The project activity includes the installation of new plants at a site where currently power or heat generation occurs. The new plant replaces or is operated next to existing plants (capacity expansion projects). Project types included under this methodology are co-generation of power and heat using biomass. Typical activities include capacity expansions, as is the the current UCR project activity.

UCR CoU Standard is used to determine the baseline grid emission factor for the 2013 - 2022 period.

Application of methodologies and standardized baselines

- The project activity is a power generation project using a biomass (bagasse) and displaces CO₂ emissions from electricity generation in power plants that are displaced due to the project activity. Since the project activity utilises biomass (bagasse) for the generation of power and supplies it to the local grid, it displaces fossil fuel (coal), and hence it meets the primary applicability criteria of the methodology.
- The project activity is a power-and-heat plant that encompasses cogeneration plants, i.e., power-and-heat plant in which at least one heat engine simultaneously generates both process heat and power. The total installed capacity of project activity is 46 MW which is acceptable as per the applied large-scale methodology.
- The installation of a new biomass residue fired power generation unit, which replaces or is operated next to existing power generation capacity fired with either



fossil fuels or the same type of biomass residue as in the project plant (power capacity expansion projects) is also included in this methodology.

- For the purposes of this methodology, heat does not include waste heat, i.e., heat that is transferred to the environment without utilization, for example, heat in flue gas, heat transferred to cooling towers or any other heat losses.
- The biomass used by the project plant is not stored for more than one year. The biomass used by the project plant is not processed chemically or biologically (e.g., through esterification, fermentation, hydrolysis, pyrolysis, bio or chemical degradation, etc.) prior to combustion.
- The Project Activity uses biomass residues from a production process (e.g., production of sugar), and the implementation of the project does not result in an increase of the processing capacity of (the industrial facility generating the residues) raw input (e.g., sugar) or in other substantial changes (e.g., product change) in this process.
- The project activity unit does not co-fire fossil fuel and/or does not exceed the limit of 25% co-firing fossil fuel criteria as per the UCR Protocol for such projects.
- Biomass generated power is used for direct grid supply and for meeting the captive needs at the facility. The project activity involves the grid-connected bagasse-based electricity generation capacity involving the installation of facilities for allowing the export of electricity to the regional grid.
- ➤ Biomass is not sourced from dedicated plantations. The existing installed turbogenerators are fired by bagasse, a by-product of the sugarcane processing and a biomass residue.
- Bagasse is burnt in boilers as generated from the sugar mill and does not require any specific technology for its preparation before combustion. No fuel preparation equipment has been installed at site for preparation of bagasse. Hence no significant energy quantities are required to prepare the biomass residues for fuel combustion.
- The project activity also does not include any GHG emissions related to the decomposition or burning of biomass. The baseline heat emissions for the project activity are not included in the project boundary nor does it claim for emission reductions from heat.



Applicability of double counting emission reductions

The biomass boilers and turbines are constructed by the project proponent within the project boundary. The biomass boilers, turbines and energy meters have unique IDs, which is visible on the units.

The UCR project activity had been registered as a VCS project activity under the title Bagasse based Co-generation Power Project at Khatauli (Project ID 101).

VCS Registration Date	15/07/2009
VCUs Issued (Period 1)	19/10/2005 – 31/03/2006
VCUs Issued (Period 2)	01/04/2006 – 18/03/2007

The UCR project activity had been registered as a CDM project activity under the title: Bagasse based Co-generation Power Project at Khatauli (Project ID 0826).

CDM Registration Date	19/03/2007
Crediting Period	19/03/2007 – 18/03/2017 (Fixed)
CERs Issued (Period 1)	59267 CERs (Period 19/03/2007 – 31/03/2008)
CERs Issued (Period 2)	50776 CERs (Period 01/04/2008-31/05/2010)
CERs Issued (Period 3)	28312 CERs (Period 01/06/2010-29/02/2012)

However the UCR project activity has never been issued voluntary carbon credits for the current 2013 - 2022 vintage years and there is no double counting of the credits envisioned. Although the Project Proponent is eligible to claim UNFCCC CDM CERs until 18/03/2017, the Project Proponent has decided not to claim any further credits under the CDM program (i.e., post 29/02/2012) and is seeking CoUs under the UCR program. Additionally, the same has been stated in the undertaking provided in the Double Counting Avoidance Assurance Document (DAA) by TEIL dated 09.08.2023.



Project boundary, sources and greenhouse gases (GHGs)

The project boundary includes the physical, geographical site(s) of:

(a) the project power plant and all power plants connected physically to the electricity system that the project activity is connected to.

Leakage Emissions (LE_y)

Leakage emissions is not applicable as the project activity does not use technology or equipment transferred from another activity.

Hence $LE_v = 0$

	Source	GHG	Included?	Justification/Explanation
		CO ₂	Included	Major source of GHG emissions
	GHG Emissions from fossil fuel in Grid Baseline	CH ₄	Excluded	Excluded for simplification. This is conservative.
	Power Generation	N ₂ O	Excluded	Excluded for simplification. This is conservative.
Baseline		CO ₂	Excluded	Excluded for simplification. This is conservative.
	Uncontrolled burning or decay of surplus biomass residue	CH ₄	Excluded	Excluded for simplification. This is conservative.
	2.01.1435 7.631446	N ₂ O	Excluded	Excluded for simplification. This is conservative.
Project Activity	Emissions from Biomass Project Activity On-site fossil fuel and electricity consumption due to the project activity (stationary or mobile)	CO ₂	Excluded	No fossil fuel / electricity is consumed at the project site due to the project activity. Biomass residue transportation using default values is applied. This is conservative.
	Transportation of biomass residue	CH ₄	Excluded	Excluded for simplification. This is conservative.
	Combustion of biomass residue for electricity and / or heat generation Storage of biomass residue	N ₂ O	Excluded	Excluded for simplification. This is conservative.



Project Emissions (PE_v)

The project emissions (PE_v) under the methodology may include:

- CO₂ emissions from transportation of biomass residue to the project site,
- CO₂ emissions from on-site consumption of fossil fuels due to project activity,
- CO₂ emissions from electricity consumption at the project site that is attributable to the project activity and
- CH₄ emissions from combustion of biomass.

where

PET_y = Default project emissions resulting from transport of biomass residues as determined by following the provisions from the TOOL12, taking into account the following transport routes:

- For biomass residues:
 - (i) If the biomass residues are consumed without further processing, the route shall include only the transport of the biomass residues between the biomass processing facility or the biomass generation site and the biomass residues utilization facility.
 - (ii) As an alternative to the monitoring of the parameters needed to calculate the emissions from the transportation, project proponents may apply the following options.
- For large-scale project activities, apply a net-to-gross adjustment of 10%, i.e., multiply the emission reductions determined based on the applied methodology by 0.9 to determine the final amount of emission reductions that can be claimed.

PEFF_{CO2}, $_{y}$ = are the CO₂ emissions during the year y due to fossil fuels co-fired by the generation facility in tons of CO₂,

 $PE_{EC,y}$ = are the CO_2 emissions during the year y due to electricity consumption at the project site that is attributable to the project activity in tons of CO_2 ,

GWP_{CH4} = is the Global Warming Potential for methane valid for the relevant commitment period and,

 $PE_{Biomass,CH4,y}$ = are the CH₄ emissions from the combustion of biomass during the year y.

The proposed project activity does not have any CO₂ emissions due to fossil fuel co-firing and from electricity consumption at site. The project activity also doesn't include the CH₄ emissions from the combustion of biomass.



Hence, $PEFF_{CO2,y} = 0$, $PE_{EC,y} = 0$ and, $PE_{Biomass,CH4,y} = 0$.

Establishment and description of baseline scenario (UCR Protocol)

The baseline scenario identified is:

Renewable energy technologies that displace technologies using fossil fuels, wherein the simplified baseline is the fuel consumption of the technologies that would have been used in the absence of the project activity, times an emission factor for the fossil fuel displaced.

The baseline emissions due to displacement of electricity are determined by net quantity of electricity generation as a result of the project activity (incremental to baseline generation) during the year y in MWh times the CO₂ emission factor for the electricity displaced due to the project activity during the year y in tons CO₂/MWh

Given that steam and electric power generation for internal consumption is part of the present project activity, emission reductions are only claimed from on-site incremental power generation that is injected to the grid. Therefore, the baseline scenario is the emission of GHG from the present electricity generation mix of the UPPCL grid in the northern region.

Emission Reductions (ERy) is the emission reduction due to the project activity is calculated as the difference between the baseline emissions and the sum of the project emissions and the leakage:

$$ER_y = BE_{y^-} (PE_{y} + LE_{y})$$

 BE_v = Baseline emissions in year y (t CO_{2e})

Where:

EG grid,y = Quantity of net electricity generation that is fed into the local grid as a result of the implementation of the project activity in year y (MWh)

 $\mathbf{EF}_{grid,y}$ = The CO₂ emission factor for grid connected power generation in year y calculated using UCR Standard emission factor (0.9 tCO₂/MWh).



 PE_y = Project activity emissions are calculated by applying a net-to-gross adjustment of 10%, i.e., multiply the emission reductions determined based on the applied methodology by 0.9 to determine the final amount of emission reductions that can be claimed.

LE_y = Leakage emissions = 0

For this methodology, it is assumed that transmission and distribution losses in the electricity grid are not influenced significantly by the project activity and are therefore not accounted for and also the UCR grid emission factor results in conservative estimates of the carbon credits.

Direct off-site emissions in the project activity arise from the biomass residue transport. However, the biomass is generated from the in-house processes pertaining to the sugar processing industry, hence, biomass residue transport is only accounted if biomass residue is imported from outside the project boundary. The same type of CO₂ emission occurs during transportation of coal from coal mines to thermal power plants (supplying power to state grid).

The biomass is collected from the nearby sources and is transported by trucks to the project site. Each truck laden with biomass is weighed on the electronic weighbridge and the corresponding readings are noted in the plant log books. For the current monitoring period no biomass residue was collected from outside, thus for this monitoring period, the value of this parameter is zero, however, using the UCR principles of conservativeness, transport emissions are calculated by applying a net-to-gross adjustment of 10%, i.e., multiply the emission reductions determined based on the applied methodology by 0.9 to determine the final amount of emission reductions. The reported values of the quantity of biomass transported can be verified against the plant records.

	Net Quantity of Electricity Supplied to the Grid in KWH													
Year	Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec	Total	
2013	21332400	16819200	20877900	12353700	0	6280200	9489300	0	0	0	0	14457600	101610300	
2014	19497300	17204100	18974400	12985500	0	0	0	0	0	0	3018600	18494400	90174300	
2015	19652100	17775000	16735500	16671000	908100	0	0	0	0	0	3880500	16742400	92364600	
2016	18635400	17808600	17657100	4501800	0	0	0	0	0	18900	14396700	20278500	93297000	
2017	17883900	16143000	16955100	14762700	270600	409200	0	0	0	2417700	17774100	19087200	105703500	
2018	19507200	18603300	18336900	18176400	12581400	0	0	0	28200	0	12843600	19545300	119622300	
2019	18306900	15909000	17195700	16952700	11458200	0	0	0	0	398700	16349400	16737900	113308500	
2020	12162300	10756200	8627100	15636300	16845900	6763200	0	0	0	1361400	18222300	19132800	109507500	
							-							
2021	18859800	17648700	18253200	18253200	14597100	0	0	0	0	76200	13084200	19153500	119925900	
2022	15423600	16361700	18458100	17444100	14816100	0	0	0	0	509100	17699700	18228000	118940400	



Year	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022
MWh										
supplied										
to the										
grid	101610.3	90174.3	92364.6	93297	105703.5	119622.3	113308.5	109507.5	119925.9	118940.4

Year	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022	Total
Baseline Emissions y (tCO2)	91449	81156	83128	83967	95133	107660	101977	98556	107933	107046	958005
Emission Reductions (0.9* BE) (tCO2)	82304	73040	74815	75570	85619	96894	91779	88700	97139	96341	862201

Total emission reductions (ER_v) = $8,62,201 \text{ tCO}_2$ (8,62,201 CoUs)

Conclusions:

Based on the audit conducted on the basis of UCR Protocol, which draws reference from UCR Standard for Baseline Grid Emission Factor, CDM UNFCCC Methodology ACM0006: Grid connected renewable electricity generation (Ver.16.0), the documents submitted during the verification including the Data, Project Concept Note (PCN) / Monitoring Report (MR), SQAC is able to certify that the emission reductions from the project - TEIL Biomass Grid Supply Power Project, Khatauli, Uttar Pradesh, India (UCR ID – 261) for the period **01/01/2013 to 31/12/2022** amounts to **8,62,201** tCO₂ (8,62,201 COUs)

Santosh Nair Lead Verifier (Signature) Praful Shinganapurkar Senior Internal Reviewer (Signature)

Date: 29/08/2023